# Development of solid phase extraction based ion exchange process for selective



# **Why Scandium is a Critical Element?**

- **No current domestic mining and no production facilities** in operation, completely dependent on imports for the past few years, which could present a potential supply chain risk
- Listed as a critical mineral by the USDOI.

# **Scandium sourcing issues**

- The shortage of primary resources is a main challenge for Sc.
- The US holds only 1% of primary sources including Sc
- Rising demand for scandium necessitates the development of efficient recovery methods from secondary resources like red mud and acid mine drainage (AMD).

# **PROBLEM STATEMENT**



- Existing purification methods (e.g., solvent extraction, precipitation) are often inefficient and environmentally harmful.
- Key issue: Iron and scandium share similar chemical properties (oxidation state, ionic radii), leading to co-extraction or co-precipitation during purification.

# **RESEARCH GOAL**

A major research gap exists in creating a process that achieves selective separation of Fe and Sc while also being environmentally conscious

"Solid-liquid extraction (SLE) is gaining attention for its proven ability to selectively separate target elements from low-concentration solutions, offering the advantages of easy regeneration and reusability"

**Hypothesis:** "In presence of excess chlorides, Fe forms anionic species while Sc forms neutral or cationic complexes. Anion exchange resins selectively adsorb Fe, leaving Sc in solution

# **RESEARCH OBECTIVES**

To develop an efficient process for the selective separation of Fe and Sc by

- Understanding the speciation in the presence of chloride ligands and adsorption mechanism
- Studying the effect of resin dosage, temperature, kinetics, adsorption isotherm









## separation of scandium and iron from low grade secondary sources Triveni Gangadari, Dr. Sarma Pisupati, Dr. Mohammad Rezaee Center for Critical Minerals, EME department, The Pennsylvania State University **EXPERIMENTAL INVESTIGATION 1. Batch adsorption experiments** • Kinetics Fe Adsorbed • Resin dosage • Temperature Chloride concentration **Concentration ratio 2.** Desorption experiments Sc Fe+Sc RESULTS **Effect of resin dosage: Effect of chloride concentration:** "1 g of resin captured most of the Fe" "Chloride concentration influence the speciation" Fe = 0.72(t)<sup>0.5</sup> + 2.66 $R^2 = 0.93$ 0.25 0.1 0.01 0.75 0.5 Chloride concentration (M g of resin/10 ml Speciation of Fe and Sc with varying chloride concentration -FeCl4--FeCl3 -FeCl2 + 60 50 -ScCl4--ScCl3 —ScCl2+ —ScCl+2 Sc+3 **% 20** Fe adsorption 2 3 4 5 6 7 8 9 10 11 12 9 10 11 12 7 8 Cl- concentration (M) Cl- concentration (M) CONCLUSIONS Adsorption mechanism: • Optimum conditions: 1g resin/10ml Cl- $\oplus$ FeCl<sub>4</sub> FeCl<sub>4</sub> Anion exchange solution, 9 M chloride, 8-hour contact Polymer Polymer $+ Cl^{-}$ suppor mechanism time. Fe recovery = 99%, Sc recovery <5% • High selectivity for Fe 998) due to |⊕ Cl- $\oplus$ Cl . FeCl<sub>3</sub> FeCl<sub>3</sub> Polymer lon association Polymer speciation differences in chloride. \_\_\_\_\_ suppor mechanism • Thermodynamic analysis shows spontaneous, slightly endothermic Fe **Effect of temperature:** Effect of Concentration ratio (Sc:Fe): Anomolous behavior adsorption. Separating agent "Adsorption is spontaneous of Sc at higher Sc:Fe is due to electrostatic interaction **Resins demonstrated >90% desorption** and slightly endothermic." between negative surface charge and Sc cationic species. (iii) 5 efficiency and reusability over 4 cycles. 8.3 8.25 🔳 Fe 📕 Sc 년 0 전 8.05 2. Imperial Mining Corporate Presentation - AUG 2022 330 300 T (K) 10:10 10:100 10:500 10:1000 10:1000 0:10000 10 1 Initial pH Project-January-2021.pdf **Kinetics:** 1) External diffusion from bulk solution to adsorbent Functional group/active site surface (Described by Pseudo first order (PFO)) 2) Internal diffusion while travelling from adsorbent surface to the pore space (Weber and Morris model) lymer support with porous channe 100















3) Chemical interaction between active site and ion of interest (*(Described by Pseudo second order (PSO)*)

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Rate of PFO = 
$$\frac{d(q_t)}{dt} = K_1 (q_e - q_t)$$
  
 $q_t = q_e (1 - \exp(-K_1 t))$   
Rate of PSO =  $\frac{d(q_t)}{dt} = K_2 (q_e - q_t)^2$   
 $q_t = \frac{(q_e^2 K_2 t)}{(1 + q_e K_2 t)}$ 

Weber and Morris model,  $q_t = K_{W\&M}\sqrt{t} + C$ 

"Adsorption is chemical reaction initially and later mixed controlled"

# **DESORPTION&REGENERATION**



"DI water was able to desorb >90% of adsorbed Fe. Resin did not lose any adsorption capacity across multiple cycles"

# **SIGNIFICANCE&FUTURE WORK**

# REFERENCES

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- 3. U.S.G.S, Mineral commodity summaries 2023: U.S. Geological Survey, 210 p. 2023 https://platinaresources.com.au/wp-content/uploads/2021/01/Platina-Scandium-

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> John and Willie Leone Family **Department of Energy and** Mineral Engineering

- Expand selective separation to other • **REEs and enhance environmental** remediation.
- Offers a sustainable solution for scandium recovery from waste sources
- Helps meet REE demand while reducing environmental harm from industrial waste.